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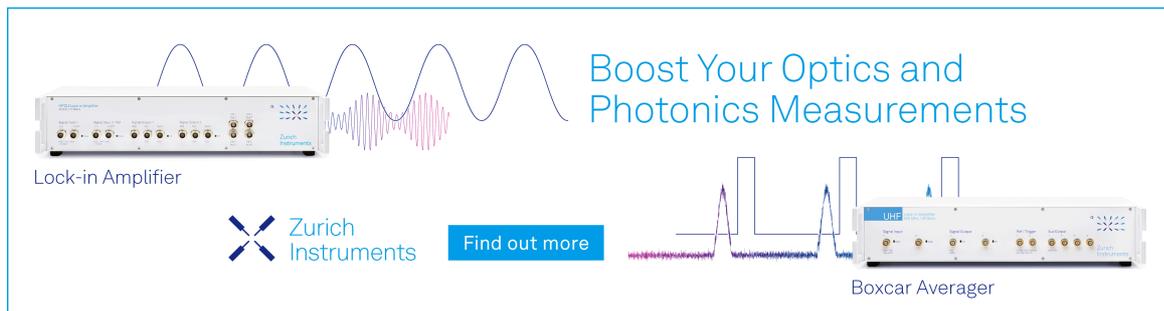


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Abstract. Galena is frequently found in association with other sulphide minerals such as sphalerite and pyrite. The pyrometallurgical methods, is commonly used for zinc recovery and requires high temperatures, resulting in heavy metal pollution and SO₂, making it unsuitable for the environment. In this study, the use of H₂SO₄ without an oxidant for direct leaching of sphalerite concentrate was investigated. The sphalerite concentrate (200 mesh) was roasted for 3 hours at 700°C to reduce the sulphur content in the sample. Following that, leaching was performed using a sulfuric acid solution with a concentration range of 1-6 mol/L for 1-5 hours. The zinc levels in the leached solution were determined using XRF (X-Ray Fluorescence) and SEM (Scanning Electron Microscopy). Before the leaching process, the particles of zinc sulphide concentrate have a clear surface and are roughly the same shape and size. The micrographs of the leaching residues show a progressive increase in the roughness of the solid as well as an increase in the amount of elemental sulphur covering the particle surfaces after the leaching process. The presence of sulfuric acid is clearly important in the leaching process, as zinc extraction rate increased with increasing sulfuric acid concentration, but only up to 3 mol/L. The highest zinc extraction, 99.17%, was obtained at 2 mol/L H₂SO₄ after 3 hours.

INTRODUCTION

Zinc is a nonferrous metal that is widely used, ranking third after aluminium and copper ^{1,2}. More than 70% of metallic zinc is currently produced from zinc sulphide concentrate via a series of roasting-leaching-electrowinning processes ³. However, zinc production has declined in recent years due to the difficulty of locating high-grade ore deposits, as well as technical and environmental issues associated with metal recovery from sulphide ores⁴. Slags, zinc dross, and filter cakes are by-products of zinc production and can be developed further as alternative sources of zinc oxide, despite their low content and complex composition ⁵.

Galena is frequently found in association with other sulphide minerals such as sphalerite (ZnS) and pyrite (FeS₂). Zinc exists primarily in the earth's crust as a sulphide, and sphalerite is most important ore. Flotation has been extensively used to separate galena and sphalerite. Zinc is concentrated using froth flotation methods due to the low solubility of zinc sulphides in acid media⁶. Flotation is the most common and commercial technique for processing nonferrous oxide minerals, as well as sulfidation with alkali metal sulphides with the addition of cationic collectors for zinc recovery. Because of the presence of adsorbed sulphide ions, the hydrophilicity of the mineral surface decreases after sulfidation⁷. However, it is less effective for zinc recovery by conventional flotation when the zinc is amorphous, such as zinc in lead slag smelting ¹.

The zinc sulphide concentrate is roasted in the first stage to produce acid-soluble zinc oxide^{8,9}. At this stage, sulphur dioxide (SO₂) is produced by the reaction of sulphur in the concentrate and air at temperatures above 900°C. As a result, in a recovery unit, SO₂ is produced, which is then converted to sulfuric acid. The calcine produced by high-temperature roasting of the sulphide concentrate is mostly zinc oxide, with about 4% zinc sulphate and a trace of zinc ferrite spinel mineral ¹⁰⁻¹³.

One of the pyrometallurgical methods, the Waelz and Ausmelt method, is commonly used for zinc recovery and requires high temperatures (1150–1250°C) in the process, resulting in heavy metal pollution, SO₂, and waste. The method appears to be economically and technically unfeasible, particularly for low-metal materials. Meanwhile, sulfuric acid leaching is the most widely used hydrometallurgical method because it is

effective in extracting zinc oxide materials, but it has drawbacks for materials containing silicates and other impurities. A large amount of silicate will dissolve and gel, preventing the zinc sulphate solution from separating¹⁴.

There has been a lot of interest in using an alternative oxidant to speed up the atmospheric leaching process and make it work in even milder conditions¹³. Several reagents, including ferric ion in chloride and sulphate media¹⁵, hydrogen peroxide, manganese dioxide, nitric acid, and others, have been used to leach sphalerite concentrate. Zinc dissolution from sphalerite in acidic ferric solution and acidic bacterial solution containing iron has received a lot of attention^{16,17}. In this study, the use of sulfuric acid without an oxidant for direct leaching of sphalerite concentrate was investigated. This study aims to compare zinc recovery in sphalerite concentrate with previous study¹³ using ozone oxidant. It can be used as a guideline for selecting reagents for leaching sphalerite concentrate on a laboratory or industrial scale.

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TABLE 1. Composition of major elements of the concentrate

<u>Element</u>	<u>Concentration (weight %)</u>
Al	1.09
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Zn	45.28
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RESULT AND DISCUSSION

The X-ray diffraction (XRD) pattern for the sphalerite concentrate is shown in Figure 1. The main compound identified was ZnS, as expected, but there were also some PbS and SiO₂ detected.

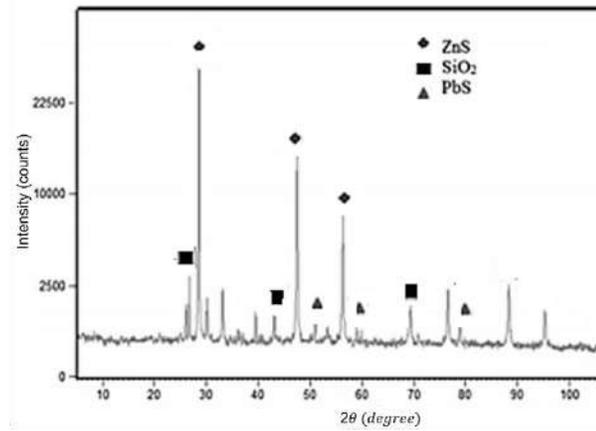


FIGURE 1. Diffractogram XRD of sphalerite concentrate

The sphalerite concentrate was then roasted for 3 hours at 700°C to reduce the sulphur content in the sample¹⁸. Temperature and time are the most important factors influencing the zinc sulphide roasting process when roasting in air and at a fixed particle size. Temperature has a greater influence on a chemically controlled process than on a diffusion-controlled reaction. Time is also an important parameter influencing the rate of oxidation and determining the capacity of the equipment. Approximately 85% of the world's zinc is produced hydrometallurgical, with the Roast-Leach-Electrowinning process dominating (RLE). The mineral sphalerite is roasted in the RLE process to make it easier to leach in sulfuric acid solution. During the roasting process, the ZnS in the concentrate is converted to zinc oxide, also known as ZnO calcine. This procedure is carried out in a 950°C furnace. The roasting reaction is an exothermic reaction that generates energy to keep the process going. This process also generates sulphur dioxide gas (SO₂), which is typically converted to sulfuric acid in a gas cleaning unit and acid plant. Chemical reactions that occur in the roasting process are indicated by reactions^{19,20}.



By varying the sulphuric acid concentration from 1 to 6 mol/L at 27±2°C, a series experiment was carried out to evaluate the effect of acid concentration on zinc dissolution efficiency. The results, as shown in the figure 2, show that the presence of sulfuric acid is clearly important in the leaching process, as zinc extraction rate increased with increasing sulfuric acid concentration, but only up to 3 mol/L.

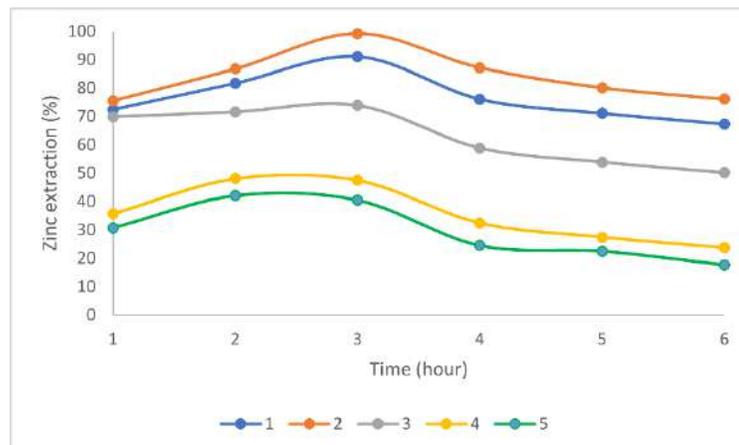


FIGURE 2. Effect of sulfuric acid concentration on zinc extraction

Zinc extractions gradually increase with leaching time and sulphuric acid concentration, indicating that sulphuric acid can dissolve a significant amount of zinc sulphide directly. In the absence of oxygen, the direct acid

dissolution of zinc sulphide produces H₂S rather than elemental sulphur. Reactions represent the chemical reactions that occur during this process. The highest zinc extraction, 99.17%, was obtained at 2 mol/L H₂SO₄ after 3 hours.



The zinc extraction rate decreased as sulfuric acid concentrations increased. This is consistent with the results of ¹³, who used ozone as an oxidant in the leaching of sphalerite concentrate. The amount of dissolved ozone decreased as the acid concentration increased. Because sulfuric acid and ozone both play important roles in zinc dissolution, it is critical to achieve an optimal balance of acid concentration and ozone solubility to maximize leaching rate. In this study, adds information about the leaching of sphalerite concentrate without oxidants, though the time required is longer than with oxidants.

Figure 3 shows the morphology of the zinc sulphide concentrates before and after leaching using SEM. Before the leaching process, the particles of zinc sulphide concentrate have a clear surface and are roughly the same shape and size (a). The micrographs of the leaching residues show a progressive increase in the roughness of the solid as well as an increase in the amount of elemental sulphur covering the particle surfaces after the leaching process (b).

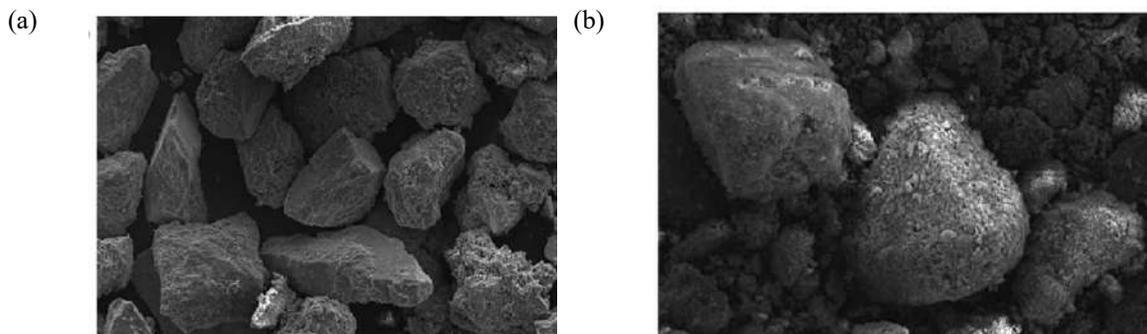


FIGURE 3. SEM images of ZnS particles (a) before leaching and (b) after leaching

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REFERENCES

- [1] R. Honaker, X. Yang, A. Chandra, W. Zhang, and J. Werner, *Extraction 2018* (Springer International Publishing, 2018).
- [2] S. Hussain, M. Khan, T.M.M. Sheikh, M.Z. Mumtaz, T.A. Chohan, S. Shamim, and Y. Liu, "Zinc Essentiality, Toxicity, and Its Bacterial Bioremediation: A Comprehensive Insight," *Front Microbiol* **13**(May), (2022).
- [3] Y.X. Zheng, J.F. Lv, H. Wang, S.M. Wen, and J. Pang, "Formation of zinc sulfide species during roasting of ZnO with pyrite and its contribution on flotation," *Sci Rep* **8**(1), 1–10 (2018).
- [4] B. Boyanov, A. Peltekov, and V. Petkova, "Thermal behavior of zinc sulfide concentrates with different iron content at oxidative roasting," *Thermochim Acta* **586**, 9–16 (2014).
- [5] I.M. Ghayad, A.L. El-Ansary, Z.A. Hamid, and A.A. El-Akshr, "Recovery of zinc from zinc dross using pyrometallurgical and electrochemical methods," *Egypt J Chem* **62**(2), 373–384 (2019).
- [6] S. Maghfouri, M.R. Hosseinzadeh, A. Rajabi, and F. Choulet, "A review of major non-sulfide zinc deposits in Iran," *Geoscience Frontiers* **9**(1), 249–272 (2018).
- [7] A.D. Titisari, S.U. Pratomo, and A. Idrus, "Hydrothermal Alteration of High Sulfidation Epithermal Deposits in

- Secang Area, Tulungagung, East Java, Indonesia,” [Journal of Applied Geology](#) **5**(2), 73 (2021).
- [8] B.S. Kim, S.B. Jeong, Y.H. Kim, and H.S. Kim, “Oxidative roasting of low grade zinc sulfide concentrate from gagok mine in Korea,” [Mater Trans](#) **51**(8), 1481–1485 (2010).
- [9] D. Amalia, T. Wahyudi, and Y. Dahlan, “The natures of zinc sulfide concentrates and its behavior after roasting process,” [Indonesian Mining Journal](#) **21**(2), 99–112 (2018).
- [10] A.A. Chen, “Kinetics of Leaching Galena Concentrates with by,” (1992).
- [11] J.C. Balarini, L. de O. Polli, T.L.S. Miranda, R.M.Z. de Castro, and A. Salum, “Importance of roasted sulphide concentrates characterization in the hydrometallurgical extraction of zinc,” [Miner Eng](#) **21**(1), 100–110 (2008).
- [12] H. Tan, J. Jin, Y. Shao, D. Zhou, Y. Zhou, Z. Wu, M. Wu, D. Shen, and Y. Long, “Microwave hydrothermal sulfidation process for zinc-containing plating sludge,” [Separation Science and Technology \(Philadelphia\)](#) **56**(17), 3001–3010 (2021).
- [13] M.Z. Mubarak, K. Sukamto, Z.T. Ichlas, and A.T. Sugiarto, “Direct sulfuric acid leaching of zinc sulfide concentrate using ozone as oxidant under atmospheric pressure,” [Minerals and Metallurgical Processing](#) **35**(3), 133–140 (2018).
- [14] Y. Zhang, Y. Hua, X. Gao, C. Xu, J. Li, Y. Li, Q. Zhang, L. Xiong, Z. Su, M. Wang, and J. Ru, “Recovery of zinc from a low-grade zinc oxide ore with high silicon by sulfuric acid curing and water leaching,” [Hydrometallurgy](#) **166**, 16–21 (2016).
- [15] N.G. Picazo-Rodríguez, M.D.J. Soria-Aguilar, A. Martínez-Luévanos, I. Almaguer-Guzmán, J. Chaidez-Félix, and F.R. Carrillo-Pedroza, “Direct acid leaching of sphalerite: An approach comparative and kinetics analysis,” [Minerals](#) **10**(4), 1–14 (2020).
- [16] K.K. Sahu, and A. Agrawal, “Lead Zinc Extraction Processes,” *Extraction of Nonferrous Metals and Their Recycling - A Training Programme*, 57–70 (2008).
- [17] S.K. Sahu, K.K. Sahu, and B.D. Pandey, “Leaching of zinc sulfide concentrate from the Ganesh-Himal deposit of Nepal,” [Metallurgical and Materials Transactions B: Process Metallurgy and Materials Processing Science](#) **37**(4), 541–549 (2006).
- [18] P. Banerjee, and P.K. Jain, “Mechanism of sulfidation of small zinc oxide nanoparticles,” [RSC Adv](#) **8**(60), 34476–34482 (2018).
- [19] J.P. Van Dyk, “An Overview of the Zincor Process,” *Southern African Pyrometallurgy* (March), 273–282 (2006).
- [20] Z. Dlamini, “Techno-economical comparison of three process routes for the treatment of Gamsberg zinc ore,” *Uct*, 140 (2015).

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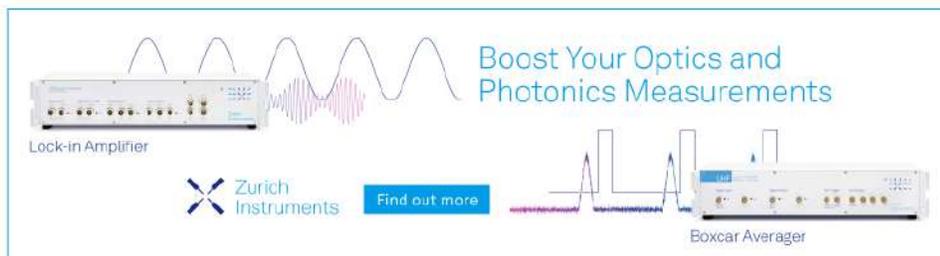
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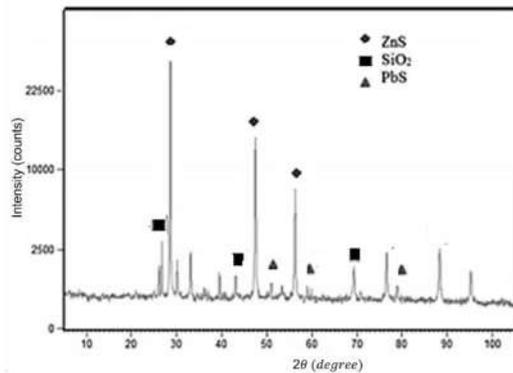
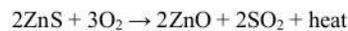


FIGURE 1. Diffractogram XRD of sphalerite concentrate

The sphalerite concentrate was **1** roasted for 3 hours at 700°C to reduce the sulphur content in the sample **1**. Temperature and time are the most important factors influencing the zinc sulphide roasting process when roasting in air and at a fixed particle size. Temperature has a greater influence on a chemically controlled process than on a diffusion-controlled reaction. Time is also an important parameter influencing the rate of oxidation and determining the capacity of the equipment. Approximately 85% of the world's zinc is produced hydrometallurgical, with the Roast-Leach-Electrowinning process dominating (RLE). The mineral sphalerite is roasted in the RLE process to make it easier to leach in sulfuric acid solution. During the roasting process, the ZnS in the concentrate is converted to zinc oxide, also known as ZnO calcine. This procedure is carried out in a 950°C furnace. The roasting reaction is an exothermic reaction that generates energy to keep the process going. This process also generates sulphur dioxide gas (SO₂), which is typically converted to sulfuric acid in a gas cleaning unit and acid plant. Chemical reactions that occur in the roasting process are indicated by reactions^{19,20}.



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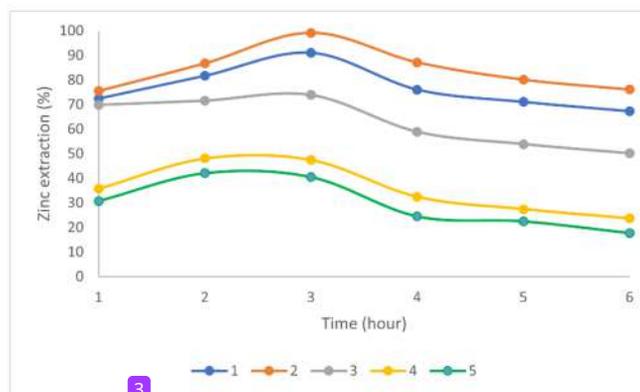
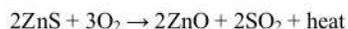


FIGURE 2. Effect of sulfuric acid concentration on zinc extraction **3**

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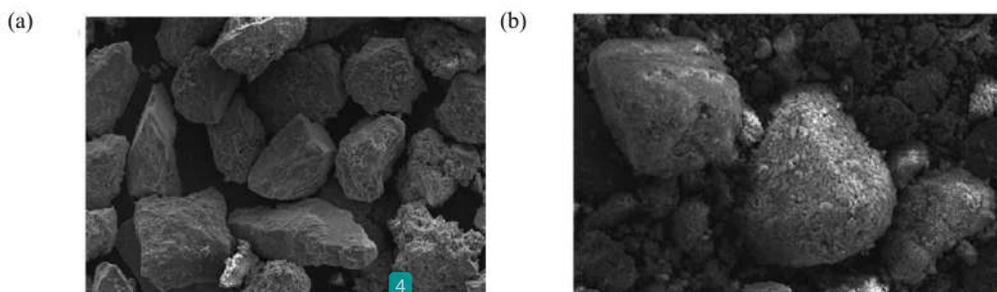


FIGURE 3. SEM images of ZnS particles (a) before leaching and (b) after leaching

CONCLUSION

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- [3] Y.X. Zheng, J.F. Lv, H. Wang, S.M. Wen, and J. Pang, "Formation of zinc sulfide species during roasting of ZnO with pyrite and its contribution on flotation," *Sci Rep* **8**(1), 1–10 (2018).
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- [5] I.M. Ghayad, A.L. El-Ansary, Z.A. Hamid, and A.A. El-Akshr, "Recovery of zinc from zinc dross using pyrometallurgical and electrochemical methods," *Egypt J Chem* **62**(2), 373–384 (2019).
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- [9] D. Amalia, T. Wahyudi, and Y. Dahlan, "The natures of zinc sulfide concentrates and its behavior after roasting process," *Indonesian Mining Journal* **21**(2), 99–112 (2018).
- [10] A.A. Chen, "Kinetics of Leaching Galena Concentrates with by," (1992).
- [11] J.C. Balarini, L. de O. Polli, T.L.S. Miranda, R.M.Z. de Castro, and A. Salum, "Importance of roasted sulphide concentrates characterization in the hydrometallurgical extraction of zinc," *Miner Eng* **21**(1), 100–110 (2008).
- [12] H. Tan, J. Jin, Y. Shao, D. Zhou, Y. Zhou, Z. Wu, M. Wu, D. Shen, and Y. Long, "Microwave hydrothermal sulfidation process for zinc-containing plating sludge," *Separation Science and Technology (Philadelphia)* **56**(17), 3001–3010 (2021).
- [13] M.Z. Mubarak, K. Sukanto, Z.T. Ichlas, and A.T. Sugiarto, "Direct sulfuric acid leaching of zinc sulfide concentrate using ozone as oxidant under atmospheric pressure," *Minerals and Metallurgical Processing* **35**(3), 133–140 (2018).
- [14] Y. Zhang, Y. Hua, X. Gao, C. Xu, J. Li, Y. Li, Q. Zhang, L. Xiong, Z. Su, M. Wang, and J. Ru, "Recovery of zinc from a low-grade zinc oxide ore with high silicon by sulfuric acid curing and water leaching," *Hydrometallurgy* **166**, 16–21 (2016).
- [15] N.G. Picazo-Rodríguez, M.D.J. Soria-Aguilar, A. Martínez-Luévanos, I. Almaguer-Guzmán, J. Chaidez-Félix, and F.R. Carrillo-Pedroza, "Direct acid leaching of sphalerite: An approach comparative and kinetics analysis," *Minerals* **10**(4), 1–14 (2020).
- [16] K.K. Sahu, and A. Agrawal, "Lead Zinc Extraction Processes," *Extraction of Nonferrous Metals and Their Recycling - A Training Programme*, 57–70 (2008).
- [17] S.K. Sahu, K.K. Sahu, and B.D. Pandey, "Leaching of zinc sulfide concentrate from the Ganesh-Himal deposit of Nepal," *Metallurgical and Materials Transactions B: Process Metallurgy and Materials Processing Science* **37**(4), 541–549 (2006).
- [18] P. Banerjee, and P.K. Jain, "Mechanism of sulfidation of small zinc oxide nanoparticles," *RSC Adv* **8**(60), 34476–34482 (2018).
- [19] J.P. Van Dyk, "An Overview of the Zincor Process," *Southern African Pyrometallurgy* (March), 273–282 (2006).
- [20] Z. Dlamini, "Techno-economical comparison of three process routes for the treatment of Gamsberg zinc ore," *Uct*, 140 (2015).

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